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# **Long-Term Demonstration of Sorbent Enhancement Additive Technology for Mercury Control**

## **Kickoff Meeting**

DOE NETL

Morgantown, WV

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Energy & Environmental Research Center

# Presentation Outline

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- Technology Introduction
- Past Experience
- Sites for this Study
  - Hawthorn Unit 5 (Kansas City Power & Light)
  - Mill Creek Unit 4 (Louisville Gas & Electric)
- Test Plan for HAW 5
- Test Plan for MC 4
- Schedule

# Sorbent Enhancement Additive (SEA) Technology

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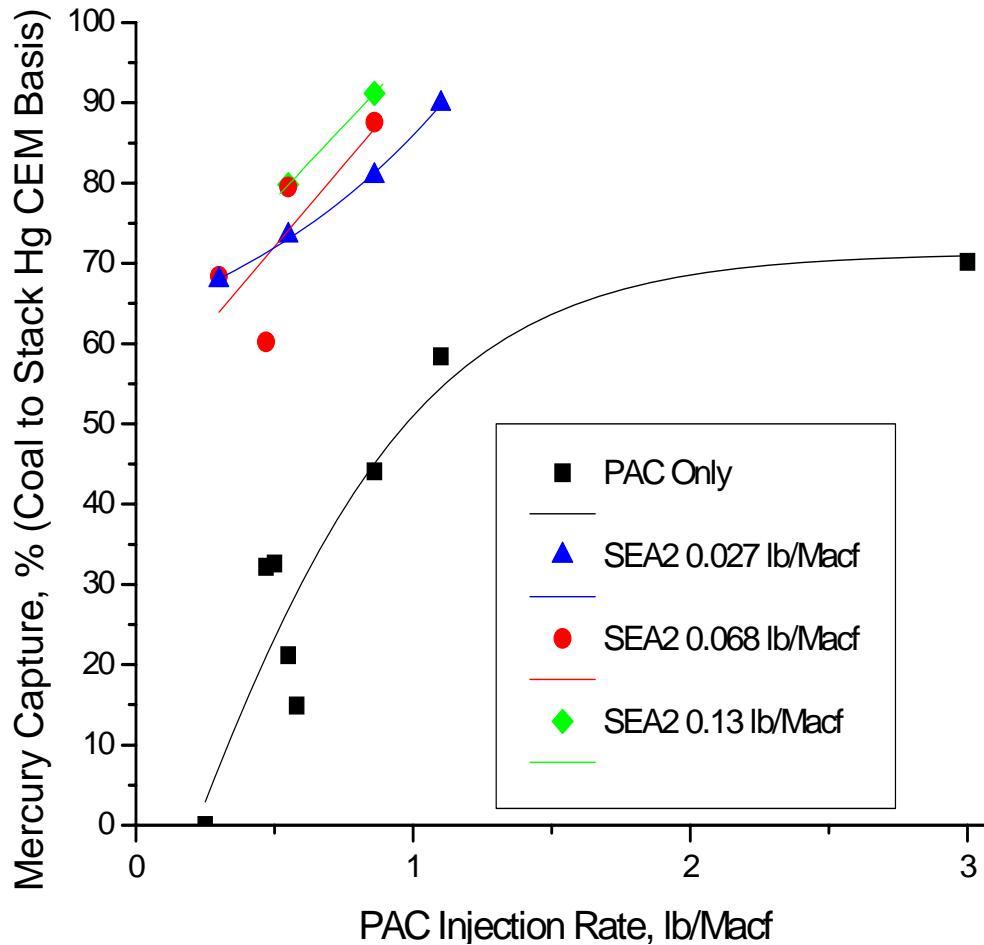
- SEA1 (B&W/Niro, U.S. patent 5,435,980)
  - Chloride added to coal feed.
  - Hg capture can be enhanced with carbon.
- SEA2 T2
  - Added upstream of the particulate control device.
  - Carbon treated in situ.
  - Tailored to desired Hg removal.

# History of SEA2 Technology

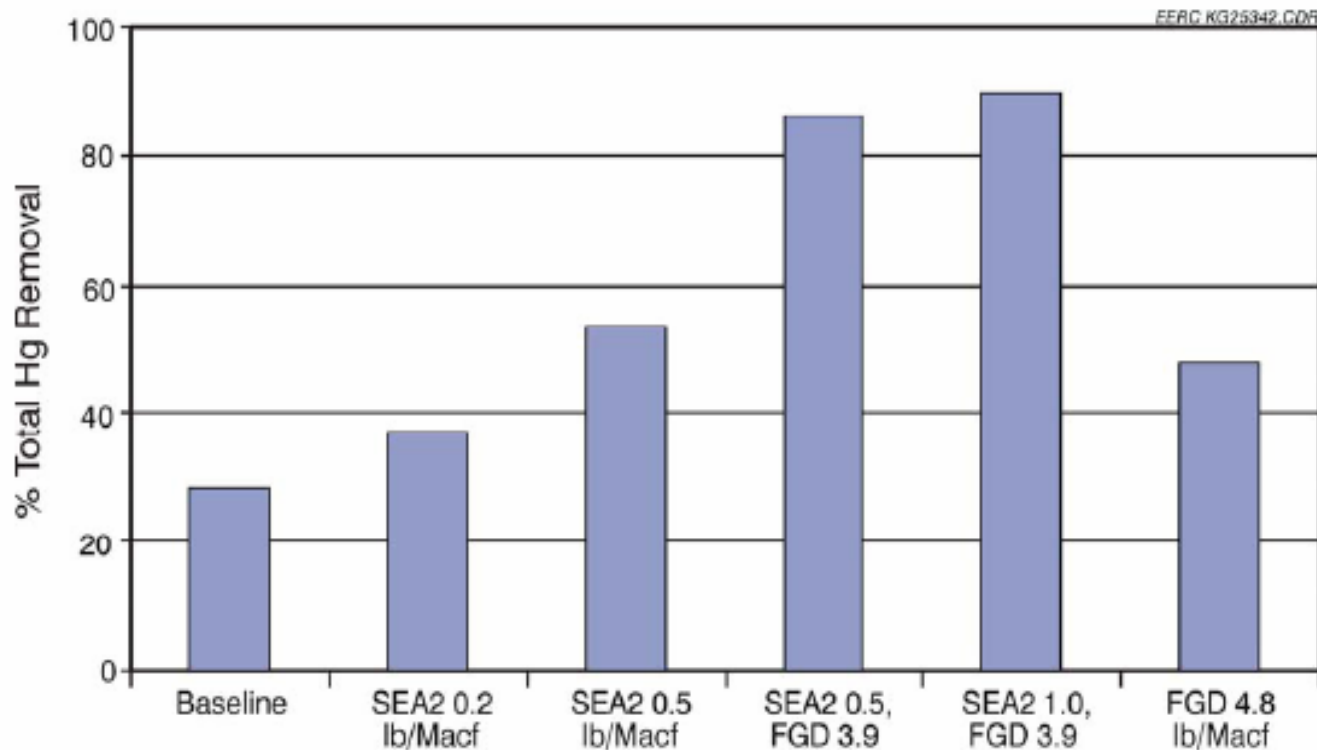
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- First testing done on ND lignite with SEA2 addition in coal.
- Later lignite tests involving co-addition with PAC in to PCD to be more effective (SEA2-T2).
- Pilot-scale projects with PRB (injection with coal) showed promise.
- Large-scale tests at Hawthorn and Hoot Lake validated SEA2-T2 effectiveness for PRB.
- All future tests conducted with SEA2-T2.

# North Dakota Lignite SDA–FF

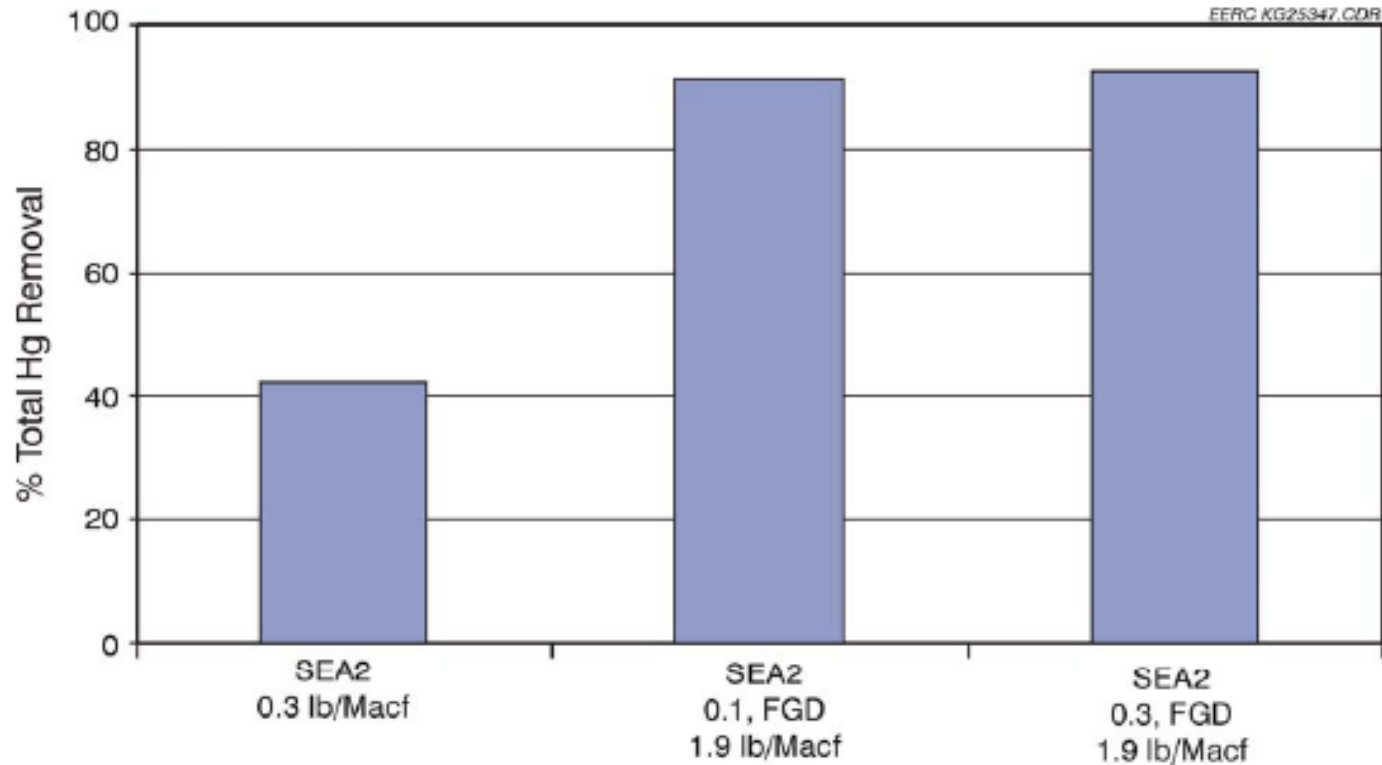


# Pilot-Scale SDA-ESP, PRB

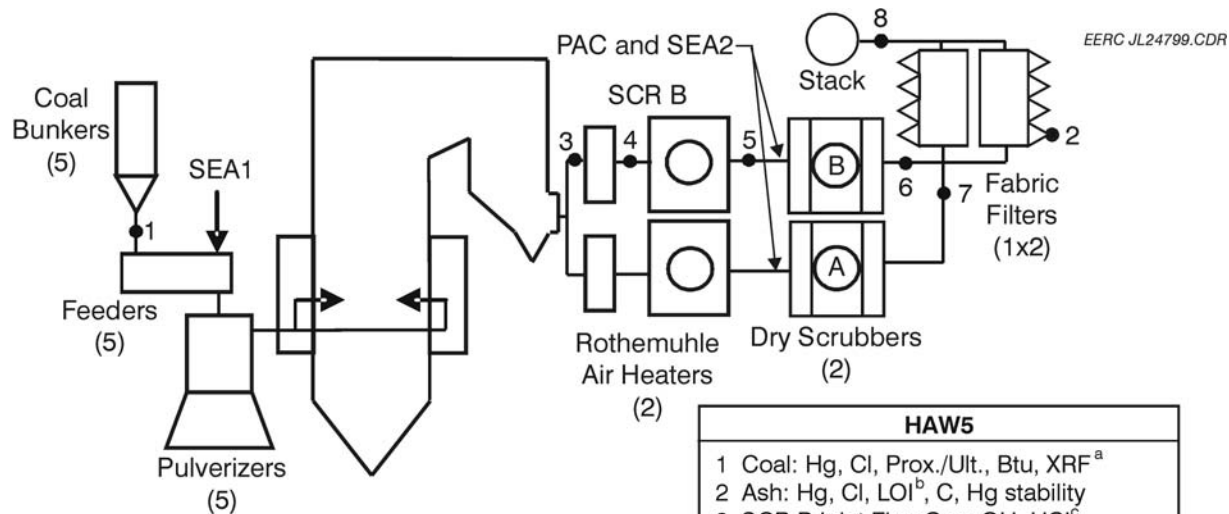


# Pilot-Scale SDA-FF, PRB

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# Hawthorn Unit 5



<sup>a</sup>X-ray fluorescence.

<sup>b</sup>Loss on ignition.

<sup>c</sup>HCl between SCR layers (Cormetech), Tests 1–4.

<sup>d</sup>HCl Test 7.

## HAW5

- 1 Coal: Hg, Cl, Prox./Ult., Btu, XRF<sup>a</sup>
- 2 Ash: Hg, Cl, LOI<sup>b</sup>, C, Hg stability
- 3 SCR B Inlet Flue Gas: OH, HCl<sup>c</sup>
- 4 SCR B Outlet Flue Gas: OH
- 5 SDA B Inlet Flue Gas: OH, CMM
- 6 SDA B Outlet Flue Gas: OH, CMM, HCl<sup>d</sup>
- 7 SDA A Outlet Flue Gas: OH, CMM, HCl<sup>d</sup>
- 8 FF Outlet Flue Gas (stack): OH, CMM



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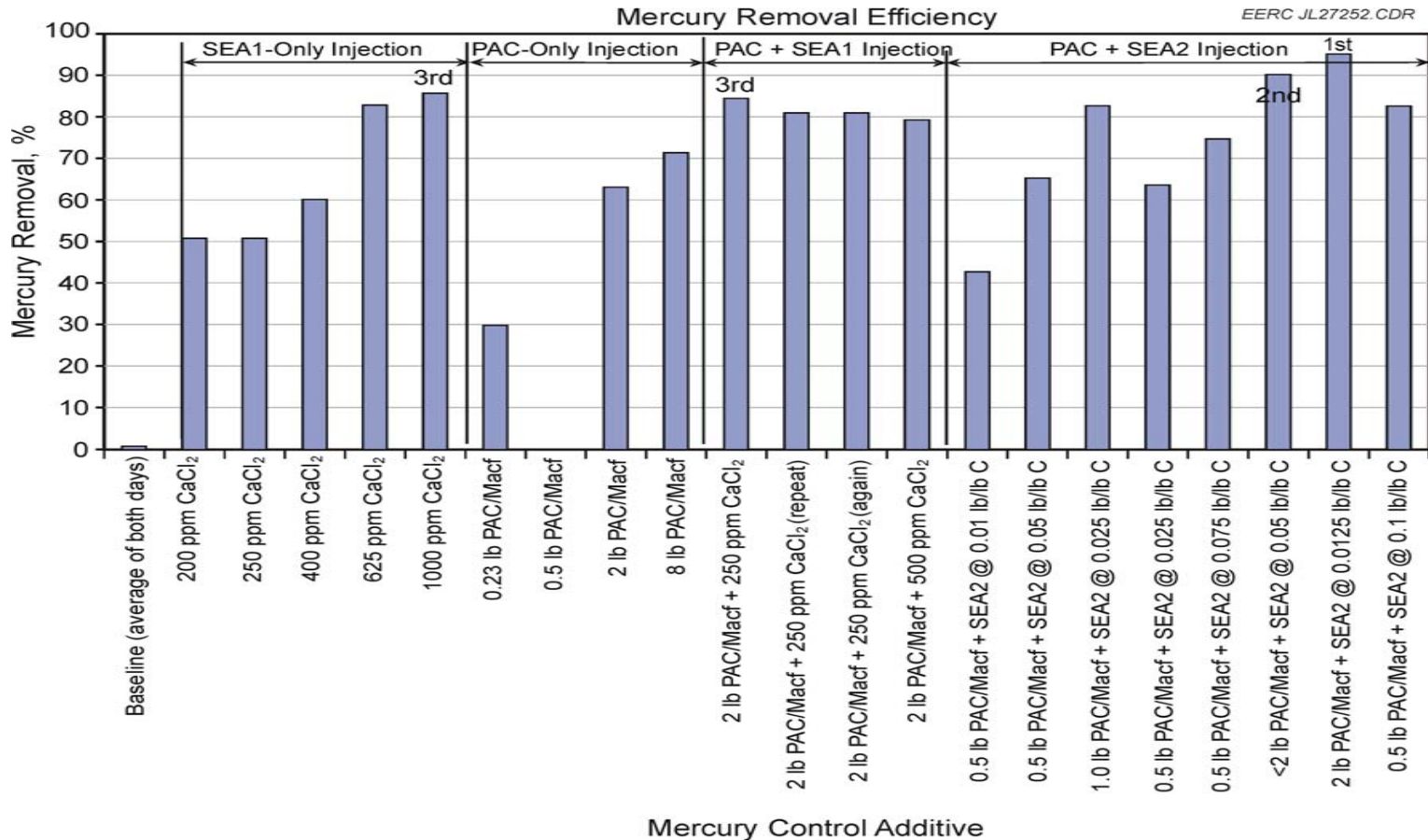
# Coal, Hg/Cl Analysis

Date	Mercury		Chlorine	
	µg/g	lb/TBtu	µg/g	lb/TBtu
7/11/2005	0.0852	7.32	6	515.82
7/12/2005	0.0955	8.20	6	515.24
7/14/2005	0.0996	8.53	7	599.73
7/15/2005	0.114	10.00	6	526.45
7/15/2005	0.0922	8.26	7	627.30
7/17/2005	0.0691	5.95	5	430.51
7/18/2005	0.0992	8.72	7	615.49
7/19/2005	0.111	9.64	6	521.10
7/20/2005	0.0956	8.38	7	613.87
7/23/2005	0.0659	5.76	6	524.61
7/24/2005	0.0711	6.31	9	798.51
7/25/2005	0.116	10.19	7	615.06
7/26/2005	0.0932	8.05	5	431.93

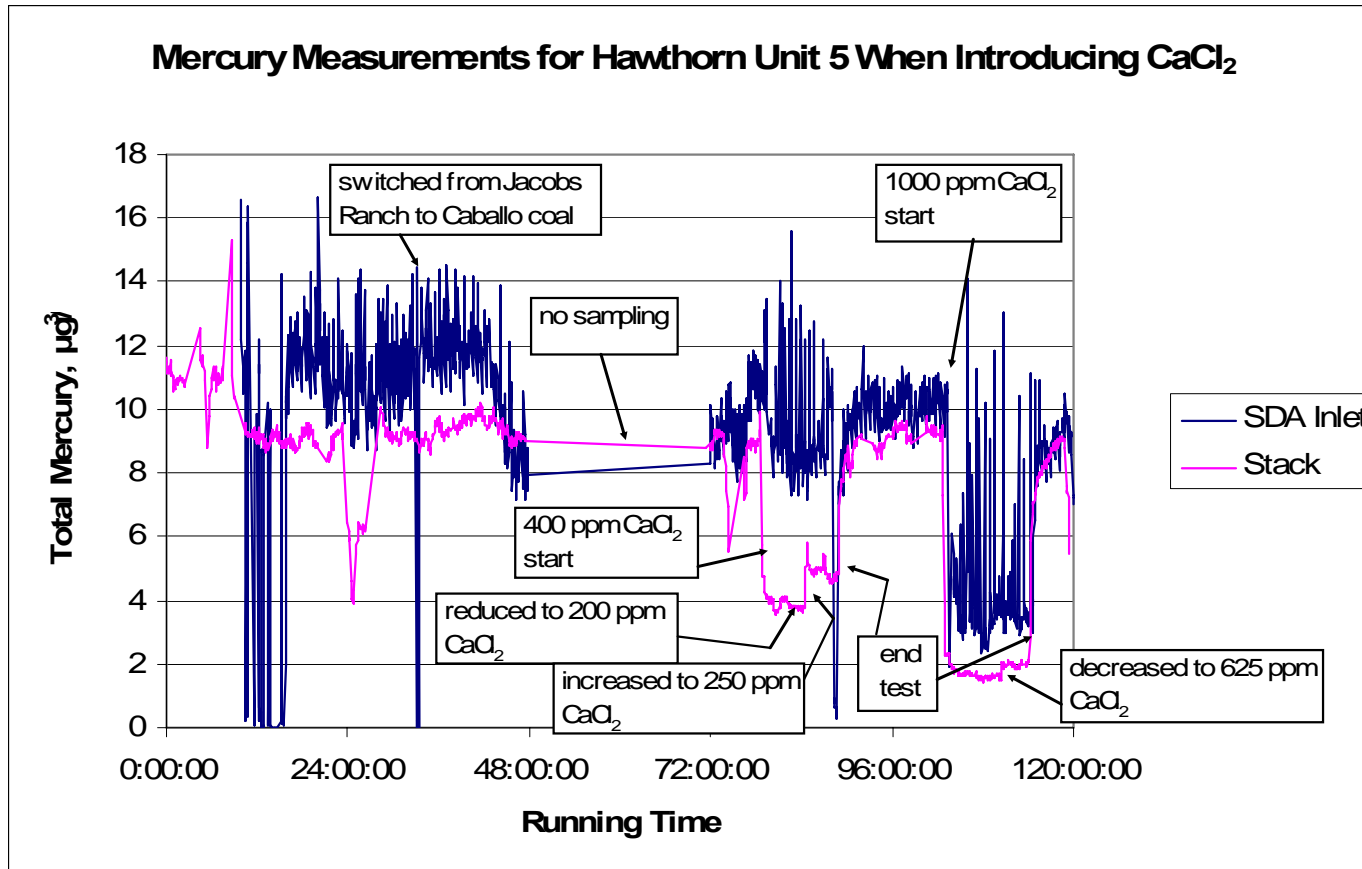
# Parametric Test Plan

Test No.	Hg Control Additive	Objective – Hg Reduction
1	None	Baseline
2	CaCl <sub>2</sub> only	400 ppmw in coal
3	CaCl <sub>2</sub> only	1000 ppmw in coal
4	PAC only	3 lb/Macf
5	PAC only	10 lb/Macf
6	CaCl <sub>2</sub> + PAC	250 ppmw, 3 lb/Macf
7	SEA2 + PAC	0.025 lb/lb, 3 lb/Macf
8	SEA2 + PAC	0.05 lb/lb, 3 lb/Macf
9	SEA2 + PAC	Vary SEA2 and PAC to determine maximum reduction
10	SEA2 + PAC	Extended test

# Hawthorn Test Results



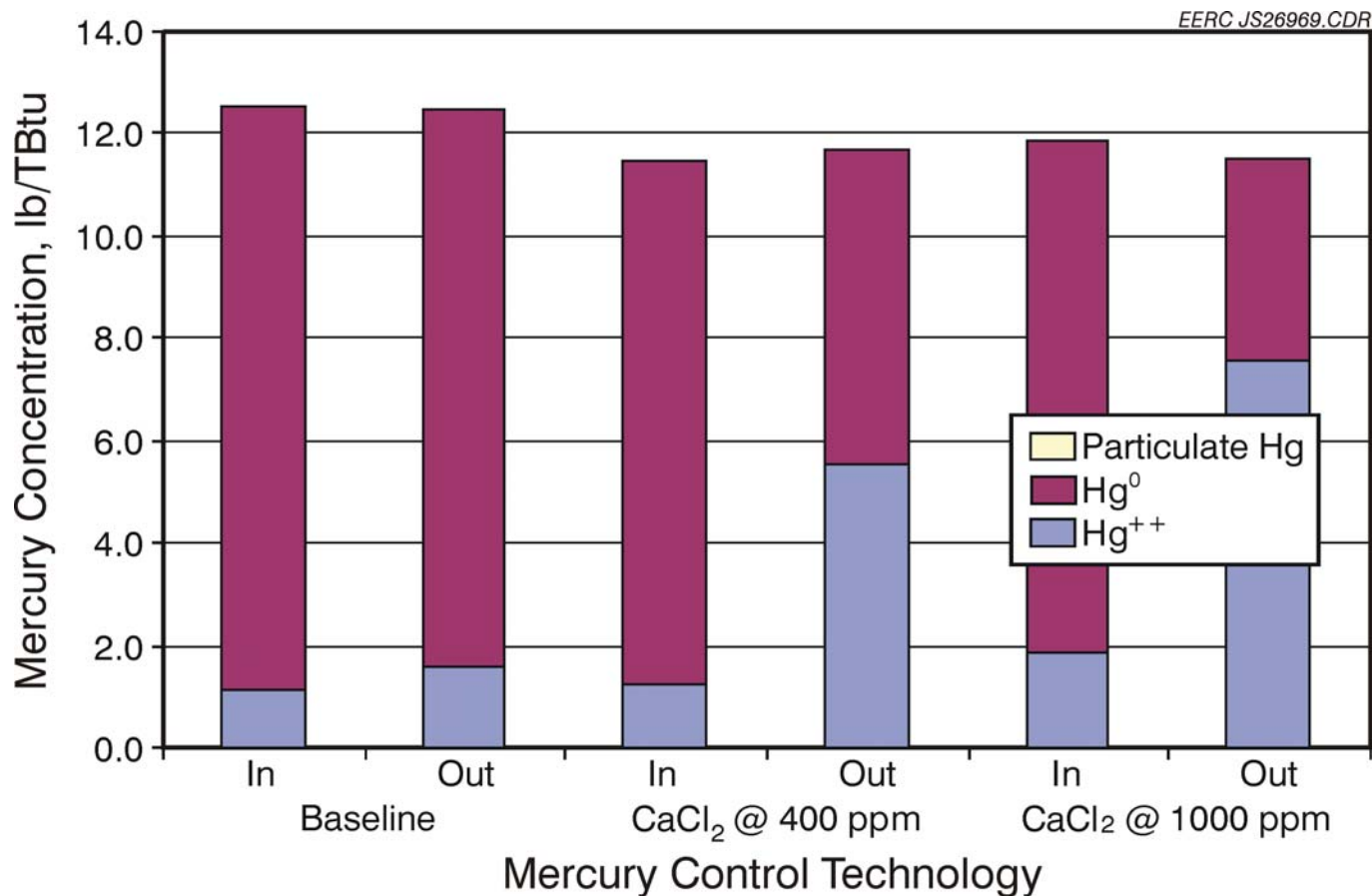
# Hawthorn Test Results (SEA1)



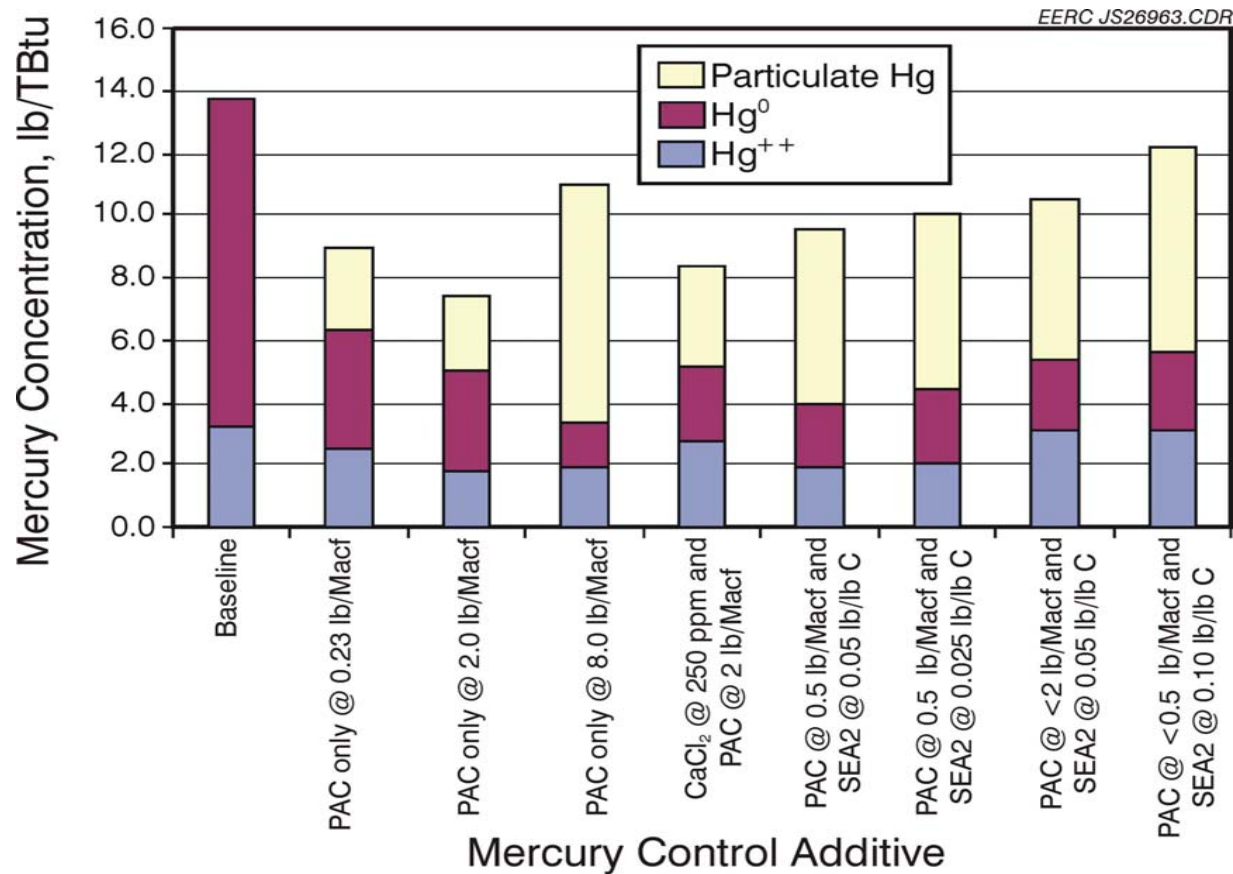
# Dust Loading at SDA Inlet

Hg Control Additive	Dust Loading, ton/TBtu	Ash Mercury Concentration, $\mu\text{g/g}$	Particulate-Bound Mercury, lb/TBtu
Baseline <sup>a</sup>	1880.6	0.385	1.45
0.23 lb PAC/Macf	2720.1	0.494	2.69
2 lb PAC/Macf	1689.6	0.698	2.36
8 lb PAC/Macf	3121.7	1.213	7.57
2 lb PAC/Macf + 250 ppm $\text{CaCl}_2$ (average of two)	2120.4	0.74	3.14
0.5 lb PAC/Macf + SEA2 @ 0.05 lb/lb C	2320.5	1.199	5.57
0.5 lb PAC/Macf + SEA2 @ 0.025 lb/lb C	2363.4	1.197	5.66
<2 lb PAC/Macf + SEA2 @ 0.05 lb/lb C	2100	1.246	5.24
0.5 lb PAC/Macf + SEA2 @ 0.1 lb/lb C	2068.5	1.591	6.58

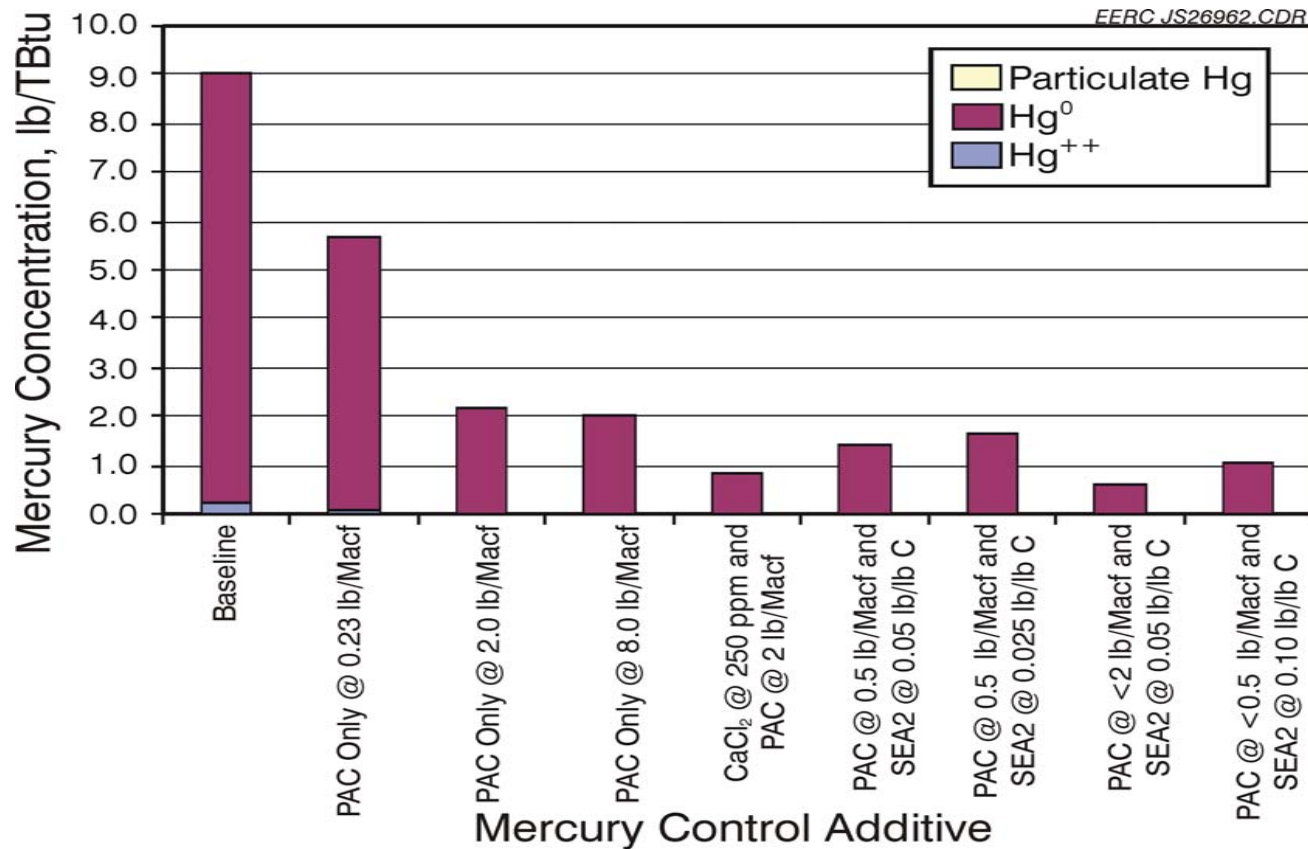
# Hg Speciation at SCR Outlet



# Hg Speciation at SDA Inlet



# Hg Speciation at Stack





# Conclusions

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- 1000 ppm Cl addition (no PAC) at Hawthorn provided an 80%+ Hg capture for 6 hours.
- >90% Hg capture was possible (for short periods of time) using SEA2 and PAC.
- >90% REDUCTION is possible with SEA2 T2 (SEA2 + PAC).

# Goals & Objectives

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- To demonstrate 90% REDUCTION in mercury emissions at Hawthorn Unit 5 and Mill Creek Unit 4.

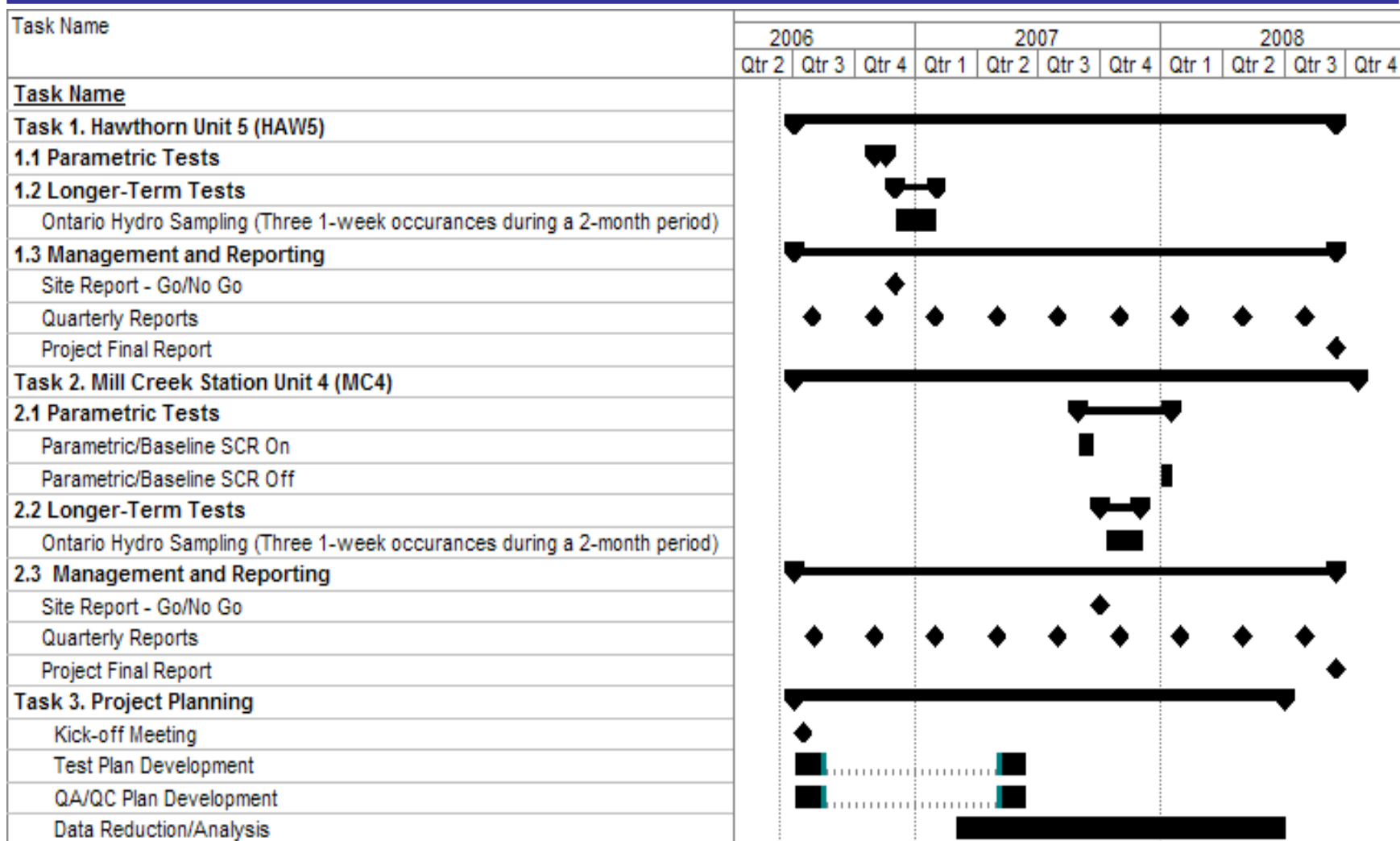
# Sites

Plant	Utility Owner	Coal	Boiler Type	Boiler Size, MW	Particulate Control	SO <sub>2</sub> Control	NO <sub>x</sub> Control
HAW5	KCP&L	PRB	Wall- fired	550	FF	SDA	LNB <sup>1</sup> , OFA <sup>2</sup> , SCR
MC4	LG&E	Eastern bituminous	Wall- fired	530	ESP/SCA= 232	Wet FGD	LNB, SCR

<sup>1</sup> Low-NO<sub>x</sub> burners.

<sup>2</sup> Overfire air.

# Task Structure/Schedule



# Test Plan for Hawthorn

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- Based on previous work the test plan for Hawthorn will concentrate on the following technologies:
  - SEA 1 Only
  - SEA 1 + PAC
  - SEA 2 T2 (SEA 2 + PAC)

# Parametric Test Plan for Hawthorn

Test #	Date	Hg Control Technology	SEA injection Location	Test	SEA 1 Coal Equiv.	SEA 2 lb/lb PAC	PAC lb/Macf
1	18-Sep	None	NA	Baseline			
	19-Sep	None	NA	Baseline			
2	20-Sep	SEA1 only (CaCl <sub>2</sub> )	Coal	Rate 1	800		
3	21-Sep	SEA1 only (CaCl <sub>2</sub> )	Coal	Rate 2	1000		
4	22-Sep	SEA1 only (CaCl <sub>2</sub> )	Coal	Rate 3	1200		
5	23-Sep	SEA1 + PAC	coal & prior to SDA	Rate 1	800		1 & 3
6	24-Sep	SEA1 + PAC	coal & prior to SDA	Rate 2	1000		1 & 3
7	25-Sep	SEA1 + PAC	coal & prior to SDA	Rate 3	1200		1 & 3
8	26-Sep	SEA2-T2 + PAC	prior to SDA	Rate 1		0.0125	1 & 3
9	27-Sep	SEA2-T2 + PAC	prior to SDA	Rate 2		0.05	1 & 3
10	28-Sep	SEA2-T2 + PAC	prior to SDA	Rate 3		0.1	1 & 3

# Mill Creek Unit 4

Sample Location	SCR Inlet, $\mu\text{g}/\text{Nm}^3$	SCR Outlet, $\mu\text{g}/\text{Nm}^3$	wet-FGD inlet, $\mu\text{g}/\text{Nm}^3$	Stack, $\mu\text{g}/\text{Nm}^3$	Reduction, %
<i>With the SCR in Service</i>					
Hg <sup>p</sup>	0.02	0.03	0.00	0.00	
Hg <sup>0</sup>	8.32	2.83	0.33	3.97	
Hg <sup>2+</sup>	0.94	5.05	7.60	0.54	
Hg <sub>total</sub>	9.27	7.90	7.93	4.50	<b>43.3</b>
<i>With the SCR Bypassed</i>					
Hg <sup>p</sup>			0.07	0.05	
Hg <sup>0</sup>			2.44	2.63	
Hg <sup>2+</sup>			6.79	0.55	
Hg <sub>total</sub>			9.30	3.23	<b>65.3</b>

# Mill Creek Unit 4 Cont.

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- Mill Creek offers challenges with the SCR in service!
  - Possibly due to reactions with  $\text{SO}_3$ .
- SEA2 T2 will be primary technology tested at Mill Creek.



# Mill Creek Test Plan SCR On

Test No.	Hg Control Technology	SEA Injection Location	Test
1	None	–	Baseline
2	SEA2 only	Prior to SCR	Rate 1
3	SEA2 only	Prior to SCR	Rate 2
4	SEA2 only	Prior to SCR	Rate 3
5	SEA2 only	Between the SCR and air heater	Rate 1
6	SEA2 only	Between the SCR and air heater	Rate 2
7	PAC only	–	1 lb/Macf
8	SEA2-T2 + PAC	Prior to SCR	Optimum SEA2-T2 + 1 lb/Macf PAC
9	SEA2-T2 + PAC	Prior to SCR	Optimum SEA2-T2 + 0.5 lb/Macf PAC
10	SEA2-T2 + PAC	Between the SCR and air heater	Optimum SEA2-T2 + 0.5 lb/Macf PAC
11–12	Contingency tests (potentially tests with B&W additive to prevent mercury reemission across the wet FGD)		

# Mill Creek Test Plan SCR Off

Test No.	Hg Control Technology	SEA Injection Location	Test
1	None	–	Baseline
2	SEA2 only	Determined from Part 1	Rate 1
3	SEA2 only	Determined from Part 1	Rate 2
4	SEA2 only	Determined from Part 1	Rate 3
5	PAC only	–	1 lb/Macf
6	SEA2-T2 + PAC	Determined from Part 1	Optimum SEA2-T2 + 1 lb/Macf PAC
7	SEA2-T2 + PAC	Determined from Part 1	Optimum SEA2-T2 + 0.5 lb/Macf PAC
8–9	Contingency tests (potentially tests with B&W additive to prevent mercury reemission across the wet FGD)		

# Sampling Locations (Both Sites)

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- Continuous Mercury Monitors – PCD inlet and stack for parametric tests. Stack only for long-term.
- Ontario Hydro – PCD inlet and stack for parametric tests and long term.
- Solid Samples – Daily coal, ash, slurry samples during parametric. Three per week during long term.
- EPA Method 5 – PCD inlet & stack?

# Project Budget

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- Total Project Cost \$2.99M
  - DOE - \$2.2M
  - B&W - \$400k
  - KCP&L - \$100k (in-kind)
  - LG&E - \$50k (in-kind)
  - Norit – 125k (in-kind)
  - SEA Supplier – \$76k (in-kind)

# Personnel

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